Increasing Iron and Reducing Phosphorous Grades of Magnetic-Roasted High-Phosphorus Oolitic Iron Ore by Low Intensity Magnetic Separation–Reverse Flotation

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Abstract: High-phosphorus oolitic iron ore, treated by suspended flash magnetic roasting, contained 42.73% iron (mainly present as magnetite) and 0.93% phosphorus (present as collophane). Low intensity magnetic separation (LIMS) was combined with reverse flotation to increase the iron and reduce the phosphorus contents of the roasted product. The results show that ideal iron ore concentration indexes of an iron ore concentrate with an iron grade of 67.54%, phosphorus content of 0.11%, and iron recovery of 78.99% were obtained under LIMS conditions employed a grind of 95% −0.038 mm and a magnetic field of 0.10 T. Optimized rougher reverse-flotation conditions used a pulp pH of 9 and dosages of ST collector, starch, and pine alcohol oil of 800 g/t, 1000 g/t, and 40 g/t, respectively; scavenging conditions used a pulp pH of 9 and dosages of ST collector, starch, and pine alcohol oil of 400 g/t, 500 g/t, and 20 g/t, respectively. Mechanism of phosphorus reduction affected result shows that the ST collector could be adsorbed on the surface of quartz after the action of starch, but adsorption was significantly weakened. The starch inhibitor negatively affected adsorption on quartz, but positively influenced adsorption of phosphorus minerals.

Keywords: suspended magnetic roast; low intensity magnetic separation (LIMS); reverse flotation; new phosphorus mineral flotation reagent; iron increase and phosphorous reduction

1. Introduction

Suspended flash magnetic roasting is a new technology for the treatment of refractory iron ore. Raw materials, such as refractory iron ores with low grade and low intensity magnetization (e.g., siderite, limonite, hematite, and goethite) or iron-containing tailings, can be processed by drying and grinding without need of pelletization. The raw material ore powder is exchanged with hot exhaust gas discharged from the magnetic roaster after a multi-stage cyclone preheater and enters the suspended magnetic roasting reaction furnace, which is characterized by its high temperature and weakly reducing atmosphere [1-3]. The fine dry mineral powder is contacted in a suspended state with CO and reacts instantaneously. The low intensity magnetic iron oxide is then converted to ferromagnetic oxide [4]. The ore powder after magnetic roasting is subjected to a multi-stage low intensity magnetic separation (LIMS) process to obtain high-grade iron concentrate products. Materials such as coal, natural gas, coal gas, and combustible exhaust gas can be used as fuel for the
suspended flash magnetic roast process [5]. Suspended flash magnetic roasting is characterized by its
high magnetization velocity, high production efficiency, high magnetic susceptibility, no need for
secondary high-temperature oxidation, high iron recovery, and sufficient resource utilization [6-7].
LIMS is often adopted to recover iron in this process, but harmful elements, such as phosphorus,
sulfur, and silicon, must still be removed by methods including reverse flotation and acid leaching
to obtain qualified iron concentrate products.

The available reserves of high-phosphorus oolitic iron ore located in Western Hubei, China,
exceed 2 billion tons. This is a chemical sedimentary iron ore, mainly composed of oolite (more than
60%) [8-9]. Specifically, the oolite consists of nuclear oolite (quartz or iron material), a collophane
girdle, hematite, and a limonite girdle; the gangue is composed of fine-grained hematite and quartz
feldspar; the cement comprises carbonate minerals and worm-like hematite. The concentrate consists
of iron-rich oolite and some hematite, and has an iron grade of up to 55% [10-12]. Phosphorus in the
ore is mainly present in the form of collophane, where the grain sizes of the collophane girdle and
monomer quartz are relatively small, as are the monomer sizes of hematite and limonite. This results
in difficult separation and lower overall iron grade. It is therefore difficult to increase the iron content
and decrease the phosphorus content.

Experimental research on a high-phosphorus oolitic iron ore containing 41.65% iron and 1.26%
phosphorus, treated by suspended flash magnetic roasting, indicated that a concentrate with an iron
grade above 60% could be produced by LIMS, but the phosphorus content exceeded 0.90% [13-15].
Compared with the phases present in the original ore, a significant increase in iron content was
observed, but phosphorus reduction was not satisfactory. It is important to accelerate the
development of high-phosphorus oolitic iron ore resources in Western Hubei, thus this work tested
the suspended flash-roasted ore using magnetic separation and reverse flotation for phosphorus
reduction. The mechanism of action of a new phosphorus mineral flotation agent, ST collector, was
also studied.

2. Materials and Methods

2.1 Sampling

High-phosphorus oolitic iron ore from Western Hubei that had been processed by suspended
flash magnetic roasting was collected as the test sample. The sample contained 42.73% iron and 0.93%
phosphorus. The main recoverable mineral in the roasted ore was magnetite. The harmful element
phosphorus mainly existed in the form of colloidal phosphate, which was characterized by its small
particle size and caused great difficulty in increasing the iron content and decreasing the phosphorus
content. The gangue minerals were mainly apatite, chlorite, quartz, and mica. The chemical
composition is shown in Table 1. Analysis of the iron phases is shown in Table 2. X-ray diffraction
phase analysis is shown in Figure 1.

<table>
<thead>
<tr>
<th>Composition</th>
<th>Fe</th>
<th>P</th>
<th>S</th>
<th>As</th>
<th>SiO2</th>
<th>CaO</th>
<th>MgO</th>
<th>Al2O3</th>
<th>K2O</th>
<th>Na2O</th>
<th>TiO2</th>
<th>V2O5</th>
</tr>
</thead>
<tbody>
<tr>
<td>Content</td>
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<td>0.93</td>
<td>0.008</td>
<td>0.006</td>
<td>15.63</td>
<td>6.12</td>
<td>0.67</td>
<td>-5.55</td>
<td>0.33</td>
<td>0.055</td>
<td>0.033</td>
<td>0.016</td>
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<table>
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<tr>
<th>Composition</th>
<th>TFe</th>
<th>Magnetite</th>
<th>Hematite</th>
<th>Pyrite</th>
<th>Ferrosilite</th>
<th>Siderite</th>
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<tr>
<td>Content</td>
<td>42.73</td>
<td>40.11</td>
<td>0.07</td>
<td>0.02</td>
<td>2.52</td>
<td>0.01</td>
</tr>
<tr>
<td>Occupancy</td>
<td>100.00</td>
<td>93.87</td>
<td>0.16</td>
<td>0.05</td>
<td>5.89</td>
<td>0.03</td>
</tr>
</tbody>
</table>
2.2. Low intensity Magnetic Separation

The suspended flash-roasted ore was ground in a conical ball mill to obtain fine powders of certain particle sizes. Magnetic and non-magnetic products were obtained using a XCGS-13 magnetic separation tube (Jinlin Exploration Machinery Plant, China) under a specified magnetic-field intensity. These were filtered, dried, weighed, sampled, and analyzed. The LIMS separation indexes were evaluated by the iron and phosphorus contents.

2.3. Reverse Flotation

Reverse flotation, aimed at reducing the phosphorus content, was carried out using an XFD-1.5L hanging tank flotation machine (Jinlin Exploration Machinery Plant, China) operating at a spindle speed of 1650 r/min. A 500 g mass of iron concentrate was added to the 1.5 L flotation tank. Distilled water (1.0 L) was added and the pulp stirred and mixed for 3 min, followed by adjustment to the required pH using sodium carbonate or sodium hydroxide. After 10 min of pulping, a flotation inhibitor and collector were added, the pulp stirred for 3 min, followed by 3 min of flotation and then froth removal. The froth (flotation tailings) and in-tank product (iron concentrate) were separately filtered, dried, and weighed. Quantitative analyses of iron and phosphorus were conducted to calculate the recoveries of iron and phosphorus.

2.4. Mechanism of Reverse Flotation

(1) Zeta Potential Measurement

The prepared magnetic iron concentrate sample of < 0.038 mm particle size was further ground using an agate mortar to obtain a powder of < 5 μm that was subjected to zeta potential measurement. In the test, 0.02 g of the ore sample was placed in a beaker, followed by addition of 40 mL of ultrapure water, adjustment of the pH value with HCl or NaOH solution, and addition of different collectors. Magnetic stirring was carried out for 10 min and the contents were then allowed to stand for 5 min. The supernatant was transferred to a Tiselius apparatus and zeta potential measurement was performed using a JS94H microelectrophoresis apparatus. Each experimental condition was measured three times and the average values are reported.

(2) Infrared Spectroscopy

Infrared spectra of the mineral surfaces before and after the action of different agents were determined using an IR Affinity 1 Fourier-Transform infrared spectrometer (Zhongshi Walker (Tianjin) Technology Development Co., Ltd, China).

An iron concentrate sample with a mass of 2 g and ground to a fineness of < 5 μm was added into the flotation tank and stirred, followed by addition of various chemicals according to the flotation test sequence. The sample was removed on completion of pulping, vacuum-filtered, and the solid product was dried in air at room temperature. A mass of 1 mg of the solid was mixed with 100 mg of spectrally pure KBr, ground with an agate mortar, and pressed into a tablet prior to analysis.
3. Results and Discussion

3.1. Low intensity Magnetic Separation

Application of the roasted ore to LIMS processing was intended to increase the iron content of
the product, given that the main iron-containing mineral was magnetite.

3.1.1. Effect of Grinding Fineness

A conical ball mill was applied to grind the suspended flash-roasted ore. A mass of 100 g was
processed using a liquid-to-solid ratio \( R = 2:1 \). Grinds with 95% passing 0.154 mm, 0.074 mm, 0.038
mm, and 0.019 mm were prepared to carry out the separation tests at different finenesses of grind.
The LIMS magnetic-field intensity \( H \) was 0.08 T. The results are shown in Figure 2.

![Figure 2](image-url)

**Figure 2.** Effect of particles size on performance of the low intensity magnetic separation

**Greater fineness is advantageous to improving** the degree of liberation of minerals. Under the
combined action of magnetic and mechanical forces during the magnetic separation process and at a
constant magnetic-field intensity, greater grinding fineness is an efficient method to improve the
concentrate grade; however, greater grinding fineness also has an adverse effect on recovery of the
concentrate. A grinding fineness of 95% –0.038 mm was suitable for achieving a magnetic product
with an iron content of 65.68% and phosphorus content of 0.68%, at an iron recovery of 85.01%.

3.1.2. Effect of Magnetic-Field Intensity

A conical ball mill was applied to grind the suspended flash-roasted ore. As above, the grinding
conditions employed 100 g ore and \( R = 2:1 \). A sample comprising 95% –0.038 mm was employed to
investigate the effects of different magnetic-field intensities. The results are shown in Figure 3.
With the increase of magnetic-field intensity, the iron grade of the magnetic product steadily decreased, along with a steady increase of iron recovery. An initial decrease and subsequent increase of the phosphorus content with increasing magnetic-field intensity was observed. A magnetic-field intensity $H$ of 0.10 T was suitable to achieve the following magnetic product indexes: iron grade of 65.06%, phosphorus content of 0.69%, and iron recovery of 87.99%.

3.2. Reverse Flotation

The objective of the reverse flotation step was to selectively float phosphorus minerals from the LIMS product and thereby achieve a reduction in the phosphorus content of the iron concentrate.

3.2.1. Effect of Collector

Lauryl amine, sodium oleate, ST collector, and a mixed amine were applied as reverse-flotation phosphorus mineral collectors on the LIMS iron concentrates. Conditions employed a Na$_2$CO$_3$-adjusted pulp pH of 8, starch dosage of 800 g/t, collector dosage of 600 g/t, and pine alcohol oil dosage of 40 g/t. The results are shown in Figure 4.
Figure 4. Effect of collector on the iron and phosphorus grades and recoveries in reverse flotation.

Using lauryl amine, sodium oleate, and the mixed amine as collectors, the iron grades of the flotation tailings exceeded 60%, which represented high losses of iron, and relatively high phosphorus contents of the iron concentrate were obtained (> 0.60%). In contrast, the ST collector had an obvious effect on phosphorus reduction: the concentrate contained an iron grade of 66.57%, phosphorus content of 0.36%, and iron recovery was 90.01%.

3.2.2. Effect of Collector Dosage

Increased dosage of the collector during a flotation process is conducive to improving recovery, but excessive dosage can easily target other minerals and affect the grade of the concentrate [16-19]. Appropriate collector dosage is not only beneficial to improving the flotation index, but also plays a key role in the regulation of operating costs. Tests were carried out using a Na$_2$CO$_3$-adjusted pulp pH of 8, starch dosage of 800 g/t, and pine alcohol oil dosage of 40 g/t. The results are shown in Figure 5.

Figure 5. Effect of ST collector dosage on iron and phosphorus grades and recoveries in reverse flotation.
With increased dosage of ST collector, the iron grade of the concentrate steadily increased, along with an initial increase and subsequent decrease in iron recovery and a regular decrease in phosphorus content. When the collector dosage increased to 1000 g/t, the phosphorus content of the concentrate was reduced to a minimum of 0.31%; at a collector dosage of 800 g/t, the phosphorus content increased by only 0.01%. These results indicated that an increase in the dosage of collector was beneficial to the reduction of phosphorus content in the iron concentrate; however, excessive collector dosage lead to an unsatisfactory effect. To improve the product indexes of the iron concentrate, it was necessary to set reasonable conditions by taking other factors into account; thus, an ST collector dosage of 800 g/t was considered ideal, yielding the following concentrate indexes: iron grade of 66.63%, phosphorus content of 0.32%, and iron recovery of 90.02%.

3.2.3. Effect of Inhibitor Dosage

Addition of an inhibitor in the flotation process improves the hydrophilicity of non-target minerals, weakens adsorption by the collector, and enhances the collection ability of the target mineral. On LIMS processing of the suspended flash-roasted ore, most of the gangue minerals entered the non-magnetic product. The main gangue components of the magnetic product were phosphorus-containing minerals [20-22]. It was necessary to inhibit flotation of magnetite during the process of reverse flotation and phosphorus reduction. Starch is the main inhibitor used for iron minerals. Starch is also a flocculant, and therefore either excessive or too little dosage has an important influence on magnetite inhibition [23-24]. Tests were carried out using a Na₂CO₃-adjusted pulp pH of 8, ST collector dosage of 800 g/t, and pine alcohol oil dosage of 40 g/t. The results are shown in Figure 6.

Figure 6. Effect of starch dosage on iron and phosphorus grades and recoveries in reverse flotation.

Increased dosage of starch was conducive to reducing the iron content of the froth product, thereby reducing the losses of iron. When the starch dosage was increased to 1000 g/t, the iron grade of the concentrate increased to 67.05%, the phosphorus content was reduced to 0.25%, and the iron recovery was 90.01%; at a starch dosage of 1200 g/t, the iron grade was reduced to 66.75%, the phosphorus content was reduced to 0.24%, and the iron recovery was 87.99%. This further indicated that excessive dosage of starch caused a certain flocculation effect in addition to its inhibition of magnetite flotation; in the absence of phosphorus-containing minerals and ST collector, this would adversely affect the quality of the iron concentrate product. A reasonable starch dosage was therefore considered to be 1000 g/t, which gave a concentrate with an iron grade of 67.05%, phosphorus content of 0.25%, and iron recovery of 90.01%.
3.2.4. Effect of Pulp pH

To achieve adsorption of the flotation agent by the target mineral, a suitable pulp pH is necessary. Tests were carried out using a Na₂CO₃-adjusted pulp pH, ST collector dosage of 800 g/t, starch dosage of 1000 g/t, and pine alcohol oil dosage of 40 g/t. The results are shown in Figure 7.

![Figure 7. Effects of pulp pH value on iron and phosphorus grades and recoveries in reverse flotation.](image)

As the pH of the pulp increased, the grade of the iron concentrate first increased and then decreased; the phosphorus content exhibited the opposite trend. If the pH is too high during a flotation process, the viscosity of the pulp increases, which is not conducive to adhesion of minerals to the froth and thus affects the separation of phosphorus minerals and magnetite. A flotation pulp pH of 9 was most suitable, achieving the following concentrate indexes: iron content of 67.11%, phosphorus content of 0.22%, and iron recovery of 90.61%.

3.2.5. Effect of Time on Reverse-Flotation Scavenging Process

As shown above, a single-rougher reverse-flotation stage was used to process the LIMS iron concentrate and ideal phosphorus reduction indexes were obtained. To further investigate whether it was possible to achieve deep dephosphorization by increasing the scavenging time and thereby provide better raw materials for iron concentrate products to steel smelters, the test flowsheet shown in Figure 8 was used to evaluate the effect of scavenging time on decreasing the phosphorus content of the product. The results are shown in Table 3.
Figure 8. Flowsheet used to investigate the effect of scavenging time of reverse-flotation step.

Table 3. Effect of scavenging time on iron and phosphorus grades and recoveries in reverse flotation (%).

<table>
<thead>
<tr>
<th>Products</th>
<th>Yield Individual</th>
<th>Yield Cumulative</th>
<th>Grade Fe</th>
<th>Grade P</th>
<th>Operating recovery Fe</th>
<th>Operating recovery P</th>
</tr>
</thead>
<tbody>
<tr>
<td>Froth product I</td>
<td>11.68</td>
<td>11.68</td>
<td>49.25</td>
<td>6.12</td>
<td>8.84</td>
<td>78.55</td>
</tr>
<tr>
<td>Froth product II</td>
<td>2.67</td>
<td>14.35</td>
<td>55.05</td>
<td>3.36</td>
<td>2.26</td>
<td>9.86</td>
</tr>
<tr>
<td>Froth product III</td>
<td>1.48</td>
<td>15.83</td>
<td>58.89</td>
<td>2.58</td>
<td>1.34</td>
<td>4.19</td>
</tr>
<tr>
<td>Iron concentrate</td>
<td>84.17</td>
<td>100.00</td>
<td>67.68</td>
<td>0.08</td>
<td>87.56</td>
<td>7.40</td>
</tr>
<tr>
<td>Totals</td>
<td>100.00</td>
<td></td>
<td>65.06</td>
<td>0.91</td>
<td>100.00</td>
<td>100.00</td>
</tr>
</tbody>
</table>

Use of a single rougher and single scavenger stage in reverse flotation of the LIMS concentrate reduced the content of harmful elemental phosphorus to less than 0.20%. Therefore, based on the overall process, one rougher and one scavenger would achieve a concentrate yield of 1.48% + 84.17% = 85.65%, with an iron grade of \( (1.48\% \times 58.89\% + 84.17\% \times 67.68\%)/(1.48\% + 84.17\%) = 67.53\% \), a phosphorus content of \( (1.48\% \times 2.58\% + 84.17\% \times 0.08\%)/(1.48\% + 84.17\%) = 0.12\% \), and an iron recovery of \( (1.34\% + 87.56\%) = 88.90\% \).

3.3. Combined Low intensity Magnetic Separation–Reverse Flotation

The LIMS–reverse-flotation method was further used to test the effect of single-pass process conditions on increasing the iron and decreasing the phosphorus contents of suspended flash-roasted high-phosphorus oolitic iron ore from Western Hubei. The test flowsheet shown in Figure 9 was employed. The results are shown in Table 4. The chemical analyses are shown in Table 5.
Figure 9. Combined test flowsheet for low intensity magnetic separation–reverse flotation process.

Table 4. Test results for low intensity magnetic separation–reverse flotation process (%).

<table>
<thead>
<tr>
<th>Products</th>
<th>Yield</th>
<th>Grade</th>
<th>Recovery</th>
</tr>
</thead>
<tbody>
<tr>
<td></td>
<td></td>
<td>Fe</td>
<td>P</td>
</tr>
<tr>
<td>Iron concentrate</td>
<td>49.98</td>
<td>67.54</td>
<td>0.11</td>
</tr>
<tr>
<td>Tailings</td>
<td>50.02</td>
<td>17.94</td>
<td>1.75</td>
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<tr>
<td>Totals</td>
<td>100.00</td>
<td>42.73</td>
<td>0.93</td>
</tr>
</tbody>
</table>

Table 5. Chemical analyses of iron concentrate obtained in single-pass low intensity magnetic separation–reverse flotation process (%).

<table>
<thead>
<tr>
<th>Composition</th>
<th>Fe</th>
<th>P</th>
<th>S</th>
<th>As</th>
<th>SiO₂</th>
<th>CaO</th>
<th>MgO</th>
<th>Al₂O₃</th>
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</thead>
<tbody>
<tr>
<td>Content</td>
<td>67.54</td>
<td>0.11</td>
<td>0.002</td>
<td>0.004</td>
<td>9.63</td>
<td>3.12</td>
<td>0.22</td>
<td>0.26</td>
</tr>
</tbody>
</table>

It is known from Tables 4 and 5 that for reverse flotation with one rougher and one scavenger gave the following iron concentrate indexes: iron grade of 67.54%, phosphorus content of 0.11%, and iron recovery of 78.99%. In addition, the contents of other impurity elements, such as sulfur, arsenic, and silicon, were also relatively low, meeting the requirements for a high-quality iron concentrate product.

3.4. Mechanism of Phosphorus Reduction Using New Phosphorus Mineral ST Collector

3.4.1. Electrodynamic Potential Analysis of Mineral Surfaces

The results of electrodynamic potential measurements of apatite, magnetite, quartz, and chlorite before and after the addition of ST collector are shown in Figure 10. The isoelectric point of apatite was 5.8; after addition of ST collector, the isoelectric point moved to 3.6, which indicated that the collector could be characteristically adsorbed on the surface of the apatite. Similarly, the isoelectric
point of magnetite was 6.8, which changed to 3.8 after addition of the collector, again indicating characteristic adsorption of ST collector on this mineral. The isoelectric point of quartz was 3.2; after the addition of ST collector, the electrodynamic potential became negative, indicating a significant change and thus characteristic adsorption of the collector on the quartz surface. The isoelectric point of chlorite was 5.8, which remained the same after the addition of ST collector, indicating no characteristic adsorption. These results showed that ST collector exhibited characteristic adsorption on the surfaces of apatite, magnetite, and quartz, but not on chlorite.

**Figure 10.** Electrodynamic potential analyses of (a) apatite, (b) magnetite, (c) quartz, and (d) chlorite mineral surfaces before and after the addition of ST collector.

### 3.4.2. Infrared Analysis of Flotation Reagents

**1. Starch**

The infrared spectrum of starch is shown in Figure 11. The starch molecule contains a large number of –OH, –CH, C=C, and C−O−C groups. The hydrogen bonding –OH stretching vibration adsorption occurred at 3419.96 cm⁻¹; the C–H stretching vibration ranged from 2750 cm⁻¹ to 3300 cm⁻¹. The –CH₃ asymmetric, –CH₂ symmetric, and –CH= symmetric stretching adsorptions occurred at 2971.43 cm⁻¹, 2917.51 cm⁻¹, and 2851.15 cm⁻¹, respectively. Stretching adsorption of non-conjugated C=C and symmetric bending adsorption of –CH₃ were found at 1631.80 cm⁻¹ and 1394.54 cm⁻¹, respectively; stretching adsorption peaks for C−O−C were found at both 1088.48 cm⁻¹ and 1047 cm⁻¹; the characteristic peak at 845.96 cm⁻¹ was assigned to the starch α-polysaccharide 2a-type adsorption.
Figure 11. Infrared spectrum of starch.

(2) ST Collector
The infrared spectrum of ST collector is shown in Figure 12. The stretching vibration of hydrogen-bonding −OH, −CH₃ asymmetric stretching, −CH₂− symmetric stretching, and −CH₂− asymmetric stretching bands occurred at 3149.35 cm⁻¹, 2297.72 cm⁻¹, 2917.51 cm⁻¹, and 2847.00 cm⁻¹, respectively. The saturated fatty-acid salt was homogenized with C=O and CO connected to the same carbon atom to form two C−O, where antisymmetric and symmetric stretching adsorption peaks occurred at 1557.14 cm⁻¹ and 1465.90 cm⁻¹, respectively. These two peaks are characteristic of fatty-acid salts. Stretching vibration adsorption peaks for C−O−C were found at 1100.92 cm⁻¹ and 1047.00 cm⁻¹; peaks attributed to the stretching vibration of non-conjugated C=C and symmetric bending of −CH₃ were found at 1644.24 cm⁻¹ and 1403.69 cm⁻¹, respectively. These results showed that ST is a fatty-acid collector.

Figure 12. Infrared spectrum of ST collector.

3.4.3. Adsorption Characteristics of Flotation Reagents on Mineral Surfaces

(1) Apatite
The infrared spectra of apatite before and after the action of ST collector are shown in Figure 13(a) and those of the combined action of starch and ST collector are shown in Figure 13(b). Figure 13(a) shows that significant change occurred in the infrared spectrum of apatite in the presence of ST collector. In addition to the apatite bands, peaks due the hydrogen-bonding −OH stretching vibration at 3143.35 cm⁻¹ and −CH₂− stretching vibrations at 2291.51 cm⁻¹ and 2847.00 cm⁻¹ in the ST spectrum also appeared at the corresponding positions, indicating adsorption of the collector on the apatite surface. In addition, a new adsorption peak appeared at 1572.50 cm⁻¹, which was shifted by...
about 15.36 cm\(^{-1}\) compared with the characteristic peak of the hydroxyl group in the ST spectrum (1557.14 cm\(^{-1}\)), indicating adsorption of ST collector on the surface of the apatite.

**Figure 13.** Infrared spectra of apatite before and after action (a- ST collector, b- Starch and ST collector)

The results shown in Figure 13(b) indicate that a significant change occurred in the infrared spectrum of apatite under the combined action of the starch inhibitor and ST collector. In addition to the apatite adsorption peaks, the stretching vibration of the hydrogen-bonding \(-\text{OH}\) found at 3419.35 cm\(^{-1}\) in the ST spectrum also appeared at the corresponding position, as well as the \(-\text{CH}_2\) stretching adsorptions at 925.69 cm\(^{-1}\) and 2842.75 cm\(^{-1}\), which shifted by 8.18 cm\(^{-1}\) and 4.25 cm\(^{-1}\), respectively. These results indicate that adsorption occurred on the apatite surface. The methylene adsorption peak on the surface of the apatite was higher after water washing, indicating that chemical adsorption of the collector molecules also occurred on the surface of apatite after the action of starch, in addition to its physical adsorption. The above analysis indicated that the ST collector is an effective collector for apatite and that starch can enhance the collection performance: apatite was enriched in the phosphorus tailings product, which was dephosphorized with anions. These results are in good agreement with the flotation results discussed earlier.

(2) Magnetite

The infrared spectra of magnetite before and after the action of ST collector are shown in Figure 14(a); those before and after the combined action of starch and ST collector are shown in Figure 14(b). Figure 14(a) indicates that significant change of the infrared spectrum of magnetite occurred in the presence of ST collector: in addition to its own bands, the stretching adsorption of the hydrogen-bonding \(-\text{OH}\) found at 3419.35 cm\(^{-1}\) in the ST spectrum and the symmetric stretching adsorption of \(-\text{CH}_2\) at 2847.00 cm\(^{-1}\) appeared at the corresponding positions. The methylene adsorption peak appeared at 2925.95 cm\(^{-1}\), shifted by 8.44 cm\(^{-1}\) compared with the spectrum of ST alone, indicating adsorption of the collector on the magnetite surface.

**Figure 14.** Infrared spectra of magnetite before and after the action (a- ST collector, b- Starch and ST collector).

Figure 14(b) shows that changes occurred in the magnetite spectrum on the addition of starch and ST collector. In addition to the adsorption peaks of magnetite itself, the relatively weak methylene adsorption peak was found at 2921.66 cm\(^{-1}\), indicating that the ST collector adsorbed on the magnetite surface, but the effect was relatively weak. After the magnetite treated with both starch and collector was water-washed, only the characteristic peak of magnetite itself appeared: there were
no adsorption peaks of the ST collector. This indicated that the ST collector only exhibited weak physical adsorption on the surface of magnetite in the presence of starch. Therefore, starch effectively inhibited the interaction between magnetite and the collector, causing magnetite to report with the floating phosphorite ore and separating it from the apatite. This finding is consistent with the results of the anion dephosphorization flotation tests.

(3) Quartz

The analogous spectra of quartz before and after the action of ST collector and the ST collector in the presence of starch are shown in Figures 15(a) and 15(b), respectively. The results shown in Figure 15(a) indicate that the infrared spectrum of quartz changed to some extent in the presence of the collector: in addition to its own bands, the symmetric stretching vibration attributed to −CH₂− at 2291.51 cm⁻¹ in the ST collector spectrum appeared at the corresponding position and methylene adsorption peaks appeared at 2794.46 cm⁻¹ and 2838.60 cm⁻¹, shifted by 4.08 cm⁻¹ and 8.40 cm⁻¹, respectively, indicating adsorption of ST collector on the surface of the quartz. The results shown in Figure 15(b) indicate that when the starch was added, in addition to the adsorption peaks of quartz itself, new adsorption peaks were observed at 2925.69 cm⁻¹ and 2842.75 cm⁻¹, which were shifted by 8.18 cm⁻¹ and 4.25 cm⁻¹, respectively, in comparison with the infrared spectrum of ST collector. This indicated that the collector adsorbed on the surface of the quartz under the action of starch and collector. After water-washing of the quartz with starch and collector ST, the symmetric stretching adsorption peak of −CH₂− at 2917.51 cm⁻¹ in the ST spectrum appeared at the corresponding position, but its intensity was weak. This indicated that the ST collector could adsorb on the quartz surface after the addition of starch, but the addition of starch obviously weakened this adsorption. These results further indicated that the presence of a starch inhibitor weakened adsorption of ST collector on quartz. Therefore, in the anion dephosphorization flotation process, a portion of quartz would enter the phosphorus tailings with the flotation froth under the action of ST collector. These results were in good agreement with the relatively high silicon content in the phosphorus tailings indicated by the dephosphorization flotation tests.

Figure 15. Infrared spectra of quartz before and after the action (a- ST collector, b- Starch and ST collector).

(4) Iron Chlorite

The analogous infrared spectra of chlorite before and after the action of collector ST alone and in combination with starch are shown in Figures 16(a) and 16(b), respectively. Figure 16(a) shows that the infrared spectra of chlorite were almost coincident before and after the action of ST collector, which indicated that adsorption of the collector on the chlorite surface was relatively weak. After the action of starch with the ST collector (Figure 16(b)), the infrared spectra of chlorite were again substantially coincident before and after the action of the flotation agents, indicating weak adsorption of both starch and ST collector on the chlorite surface. After the chlorite treated with starch and ST collector was water-washed, weakening intensity of the fingerprint peaks was observed. These results showed that adsorption between starch and ST collector and chlorite was weak: chlorite therefore mainly deported with magnetite during reverse-flotation dephosphorization.
Figure 16. Infrared spectra of chlorite before and after the action (a- ST collector, b-Starch and ST collector).

4. Conclusions

1) High-phosphorus oolitic iron ore from Western Hubei that was treated by suspended flash magnetic roasting contained 42.73% iron and 0.93% phosphorus. The main valuable element was iron, present as magnetite; the harmful element phosphorus existed in the roasted ore in the form of francolite (collophane); the gangue minerals were mainly apatite, chlorite, quartz, and mica.

2) The suspended flash magnetic-roasted high-phosphorus oolitic iron ore was processed by LIMS followed by reverse flotation. ST flotation reagent was added as a high-efficiency collector for reverse flotation of the phosphorus minerals. Significant iron increase and phosphorus reduction in the concentrate grades were obtained from this combined process. Reverse flotation using a single rougher and single scavenger stage yielded the following of iron ore concentrate indexes: iron grade of 67.54%, phosphorus content of 0.11%, and iron recovery of 78.99%. In addition, the contents of other impurity elements in the concentrate, such as sulfur, arsenic, and silicon, were also relatively low, meeting the requirements for a high-quality iron concentrate product.

3) Study of the mechanism of phosphorus flotation by ST indicated characteristic adsorption peaks of the collector on the surfaces of apatite, magnetite, and quartz, but not on chlorite. Infrared analyses indicated that the ST collector could adsorb on the surface of quartz after the addition of starch, but the adsorption was obviously weakened, indicating that the presence of starch inhibitor weakened the adsorption between ST collector and quartz. Adsorption of starch and ST collector on the surface of chlorite was weak.

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